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# Numerical Solution for Plane Stagnation Point Flow

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## **Abstract**

The plane stagnation point flow, where a fluid stream impinges perpendicularly on a flat surface, is a classic problem in fluid dynamics with significant theoretical and practical implications. This report presents a comprehensive numerical solution to the plane stagnation point flow using the fourth order Runge-Kutta approximation. The numerical approach is developed to solve the governing Hiemenz Flow equation.

Key flow characteristics, including velocity, are analyzed, offering insights into the fluid behavior near the stagnation point.

**Keywords:** Similarity; Plane Stagnation; Hiemenz Flow; Runge-Kutta

# **1. Introduction**

The study of fluid flow behavior near stagnation points is of paramount importance in both theoretical and applied fluid dynamics. A plane stagnation point flow, characterized by the deceleration of a fluid as it impinges perpendicularly on a surface, is a fundamental problem with wide-ranging applications in aerodynamics, thermal management, and various engineering processes. Understanding the flow characteristics in this region is crucial for optimizing performance and ensuring stability in systems where such flow conditions are encountered.

This study aims to develop and validate a robust numerical solution for the plane stagnation point flow using the fourth order Runge-Kutta approximation. The results obtained will not only enhance our theoretical understanding but also offer practical insights for applications in engineering design and optimization.

The following sections will detail the mathematical formulation of the problem and the numerical methods employed. Through this work, we aim to contribute to the ongoing advancement of numerical fluid dynamics and its application to stagnation point flow phenomena.

# **2. Problem Description**

The similarity solution for Hiemenz flow can be expressed by the non-dimensional stream function  $F(\eta)$  satisfying the ordinary differential equation

$$
F''' + FF'' + 1 - F'2 = 0
$$

subject to the boundary conditions

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$$
F(0) = 0
$$
;  $F'(0) = 0$ ;  $F'(\infty) = 1$ 

This is known as a two-point boundary value problem since the conditions are imposed at two different locations. However, for simplicity we replace  $[0, \infty]$  by a finite interval of  $\eta = 4.8$ 

The above ODE may be re-cast into a system of 3 coupled first order equations. Thus, defining the variables  $Y1 = F$ ,  $Y2 =$  $F'$  and  $Y3 = F''$ , we obtain

$$
\frac{dY_1}{d\eta} = Y_2
$$

$$
\frac{dY_2}{d\eta} = Y_3
$$

$$
\frac{dY_3}{d\eta} = Y_2^2 - Y_1Y_3 - 1
$$

with the boundary conditions  $Y1(0) = 0$ ,  $Y2(0) = 0$  and  $Y2(\infty) = 1$ .

Since Y3(0) is unknown we can guess a value for it and integrate the system forward from  $\eta = 0$  by solving the ODEs posed as initial-value problems until the condition  $Y2(\infty) = 1$  is satisfied.

We will also develop a program that iteratively guesses the correct value of Y3(0) that satisfies the condition Y2( $\infty$ ) = 1 within some prescribed tolerance level

## **3. Methodology**

This problem shall be solved numerically using the fourth order Runge-Kutta approximation. We shall carry out numerical integration of the coupled first order ODEs with prescribed initial conditions.

MATLAB codes shall be developed to solve for F and obtain results for F and its derivatives in tabulated and graphical forms. Comment statements shall be provided to show the logic of the algorithm.

MATLAB code shall also be developed that iteratively guesses the correct value of Y3(0) that satisfies the condition  $Y2(\infty) = 1$  within some prescribed tolerance level. This shall be embedded within the main program.

A discussion of the physical implications of the results and implications for the velocity components shall be provided. A summary of results: tables and plots, shall also be presented as part of the report.

#### **4. Numerical Solution**

Given the third order ordinary differential equation for Hiemenz flow

$$
F''' + FF'' + 1 - F'2 = 0
$$

subject to the boundary conditions

$$
F(0) = 0
$$
;  $F'(0) = 0$ ;  $F'(\infty) = 1$ 

We define new variables:  $Y1 = F$ ,  $Y2 = F'$  and  $Y3 = F''$ , and obtain the following set of first order coupled ODEs

$$
\frac{dY_1}{d\eta} = Y_2
$$

$$
\frac{dY_2}{d\eta} = Y_3
$$

$$
\frac{dY_3}{d\eta} = Y_2^2 - Y_1Y_3 - 1
$$

with the boundary conditions  $Y1(0) = 0$ ,  $Y2(0) = 0$  and  $Y2(4.8) = 1$ .

The boundary condition Y2( $\infty$ ) is approximated as Y2(4.8) = 1 since it will be difficult to define infinity on a computer.

The numerical integration is done using the fourth order Runge-Kutta method with an interval size of h = 0.0005. The Runge-Kutta approximation is expressed as:

$$
y_{n+1} = y_n + \frac{1}{6}k_1 + \frac{1}{3}k_2 + \frac{1}{3}k_3 + \frac{1}{6}k_4 + O(h_5)
$$
  

$$
k_1 = hf(x_n, y_n)
$$
  

$$
k_2 = hf(x_n + \frac{1}{2}h, y_n + \frac{1}{2}k_1)
$$
  

$$
k_3 = hf(x_n + \frac{1}{2}h, y_n + \frac{1}{2}k_2)
$$
  

$$
k_4 = hf(x_n + h, y_n + k_3)
$$

Using successive guesses, we obtain a value of Y3(0) = 1.232 that satisfies the boundary condition Y2(4.8)  $\approx$  1. The code is provided below.

clear;

clc;

% Define Parameters  $a = 0$ ; % lower limit of integration  $b = 4.8$ ; % upper limit of integration h = 5E-4; % step size  $n = (b-a)/h+1$ ; % number of points % Define Initial Conditions  $Y1(1) = 0;$  $Y2(1) = 0$ ;  $Y3(1) = 1.232$ ; % obtained by iteration % Define the system of ODE function handle  $eta(1) = 0;$  $f1 = \omega(Y2)$  Y2;  $f2 = \omega (Y3) Y3;$ f3 = @(Y2,Y3,Y1) Y2\*Y2-Y1\*Y3-1 % 4th Order Runge-Kutta Loop for  $i = 1:n-1$  $eta(i+1) = i*h;$  $k1_1 = h * \text{fewal}(f1, Y2(i));$  $k2_1 = h * \text{fewal}(f1, Y2(i) + k1_1/2);$  $k3_1 = h * \text{fewal}(f1, Y2(i) + k2_1/2);$  $k4_1 = h * \text{fewal}(f1, Y2(i) + k3_1);$  $Y1(i+1) = Y1(i)+(1/6)*(k1_1+2*k2_1+2*k3_1+k4_1);$  $k1_2 = h * \text{fewal}(f2, Y3(i));$  $k2_2 = h * \text{fewal}(f2, Y3(i) + k1_2/2);$  $k3_2 = h * \text{fewal}(f2, Y3(i) + k2_2/2);$ k4\_2 = h\*feval(f2,Y3(i)+k3\_2); Y2(i+1) = Y2(i)+(1/6)\*(k1\_2+2\*k2\_2+2\*k3\_2+k4\_2);  $k1_3 = h * \text{fewal}(f3, Y2(i), Y3(i), Y1(i));$  $k2_3 = h * \text{fewal}(f3, Y2(i) + k1_1/2, Y3(i) + k1_2/2, Y1(i) + k1_3/2);$  $k3_3 = h*fewa[(3,Y2(i)+k2_1/2,Y3(i)+k2_2/2,Y1(i)+k2_3/2);$ k4\_3 = h\*feval(f3,Y2(i)+k3\_1,Y3(i)+k3\_2,Y1(i)+k3\_3);  $Y3(i+1) = Y3(i)+(1/6)*(k1_3+2*k2_3+2*k3_3+k4_3);$ 

end

% Plot results plot(eta,Y2) title("Plot of \eta versus Y2") grid on xlabel('\eta') ylabel('Y2')



**Figure 1** Plot of first derivative of non-dimensional stream function

## $Y2(4.8) = 1$

Next, we develop MATLAB code that iteratively determines the correct value of Y3(0) that satisfies the condition Y2(4.8)  $= 1$  within a tolerance level of 1 x 10-3.

The code proposes a new function as follows.

$$
g = Y_2(\eta = 4.8)
$$

The value of the function, g, depends on the initial value of Y3.

$$
g = g[Y_3(0)]
$$

This function approximately becomes 1 when the true value of Y3(0) is approached, thus, the following equation is satisfied.

$$
g[Y_3(0)] - 1 = 0
$$

The code then obtains corresponding values of g for values of Y3(0) within the interval [0:2] using steps of 0.001, which is the desired level of accuracy.

A plot of the function g[Y\_3 (0)]-1 is made against Y\_3 (0). The desired value of Y\_3 (0) occurs where the curve crosses the x-axis. This value is  $Y_3$  (0)=1.2320, which is the same as earlier obtained by iteration.

A breakdown of the code is provided below.

clear;

clc;

% Define Parameters a = 0; % lower limit of integration  $b = 4.8$ ; % upper limit of integration  $h = 5E-4$ ; % step size  $n = (b-a)/h+1$ ; % number of points % Define Initial Conditions  $Y1(1) = 0;$  $Y2(1) = 0$ :  $p = 1:1E-3:2;$  $r = length(p);$ for  $i = 1:r$  $Y3(1) = p(j);$ % Define the system of ODE function handle  $eta(1) = 0;$  $f1 = \omega(Y2)$  Y2;  $f2 = \omega(Y3) Y3$ ;  $f3 = \omega(Y2, Y3, Y1) Y2*Y2-Y1*Y3-1;$ % 4th Order Runge-Kutta Loop for  $i = 1:n-1$  $eta(i+1) = i*h;$  $k1_1 = h * \text{feval}(f1, Y2(i));$  $k2_1 = h * \text{fewal}(f1, Y2(i) + k1_1/2);$  $k3_1 = h * \text{fewal}(f1, Y2(i) + k2_1/2);$ k4\_1 = h\*feval(f1,Y2(i)+k3\_1); Y1(i+1) = Y1(i)+(1/6)\*(k1\_1+2\*k2\_1+2\*k3\_1+k4\_1);  $k1_2 = h * \text{fewal}(f2, Y3(i));$  $k2_2 = h * \text{fewal}(f2, Y3(i) + k1_2/2);$  $k3_2^2 = h*$ feval(f2,Y3(i)+ $k2_2^2$ );  $k4_2 = h * \text{fewal}(f2, Y3(i) + k3_2);$ Y2(i+1) = Y2(i)+(1/6)\*(k1\_2+2\*k2\_2+2\*k3\_2+k4\_2); k1\_3 = h\*feval(f3,Y2(i),Y3(i),Y1(i));  $k2_3 = h*$ feval(f3,Y2(i)+k1\_1/2,Y3(i)+k1\_2/2,Y1(i)+k1\_3/2);  $k3_3 = h*fewal(f3,Y2(i)+k2_1/2,Y3(i)+k2_2/2,Y1(i)+k2_3/2);$  $k4_3 = h*fewal(f3,Y2(i)+k3_1,Y3(i)+k3_2,Y1(i)+k3_3);$  $Y3(i+1) = Y3(i)+(1/6)*(k1_3+2*k2_3+2*k3_3+k4_3);$ end  $q(j) = Y2(end);$ end  $qi = 1$ :  $\overline{Y3}$ <sub>-0</sub> = interp1(q,p,qi) % Plot results plot (p,q-1) xlabel('Y3(\eta=0)') ylabel('Y2(\eta=4.8) - 1')

axis([1 2 -10 50]); grid on grid minor



**Figure 2** Plot of first derivative vs second derivative of stream function

 $Y3(0) = 1.2320$ 

Finally, the subroutine that produces Y1, Y2 and Y3 is embedded within the iterative loop that solves for the correct value of Y3(0) that satisfies the boundary condition of  $Y2(4.8) = 1$ . The final code is shown below.

clear;

clc;

```
% Define Parameters
a = 0; % lower limit of integration
b = 4.8; % upper limit of integration
h = 5E-4; % step size
n = (b-a)/h+1; % number of points
% Define Initial Conditions
Y1(1) = 0;Y2(1) = 0;% Loop for boundary condition Y3(0)
p = 1:1E-3:2;r = length(p);for j = 1:rY(1) = p(j);eta(1) = 0;f1 = \omega(Y2) Y2;
f2 = \omega(Y)Y;f3 = @(Y2,Y,Y1) Y2*Y2-Y1*Y-1;
for i = 1:n-1eta(i+1) = i*h;k1_1 = h * \text{fewal(f1,Y2(i))};k2_1 = h * \text{fewal}(f1, Y2(i) + k1_1/2);k3_1 = h * \text{fewal}(f1, Y2(i) + k2_1/2);k4_1 = h*feval(f1,Y2(i)+k3_1);
 Y1(i+1) = Y1(i)+(1/6)*(k1_1+2*k2_1+2*k3_1+k4_1);
k1_2 = h * \text{feval}(f2,Y(i));k2_2 = h * \text{fewal}(f2, Y(i) + k1_2/2);k3_2 = h * \text{fewal}(f2, Y(i) + k2_2/2);k4_2 = h * \text{fewal}(f2, Y(i) + k3_2);
```

```
Y2(i+1) = Y2(i)+(1/6)*(k1_2+2*k2_2+2*k3_2+k4_2);k1_3 = h * \text{fewal}(f3, Y2(i), Y(i), Y1(i));k2_3 = h*feval(f3,Y2(i)+k1_1/2,Y(i)+k1_2/2,Y1(i)+k1_3/2);
k3_3 = h*feval(f3,Y2(i)+k2_1/2,Y(i)+k2_2/2,Y1(i)+k2_3/2);
k4_3 = h*feval(f3,Y2(i)+k3_1,Y(i)+k3_2,Y1(i)+k3_3);
Y(i+1) = Y(i)+(1/6)*(k1_3+2*k2_3+2*k3_3+k4_3);end
q(j) = Y2(end);end
qi = 1;Y3(1) = interp1(q,p,qi);
% Define the system of ODE function handle
eta(1) = 0;f1 = \omega(Y2) Y2;
f2 = \omega(Y3) Y3;
f3 = @(Y2,Y3,Y1) Y2*Y2-Y1*Y3-1;
% 4th Order Runge-Kutta Loop
for i = 1:n-1eta(i+1) = i*h;k1_1 = h*fewal(f1,Y2(i));k2_1 = h * \text{fewal}(f1, Y2(i) + k1_1/2);k3_1 = h*feval(f1,Y2(i)+k2_1/2);
k4_1 = h * \text{fewal}(f1, Y2(i) + k3_1);Y1(i+1) = Y1(i)+(1/6)*(k1_1+2*k2_1+2*k3_1+k4_1);k1_2 = h * \text{feval}(f2,Y3(i));k2_2 = h * \text{fewal}(f2, Y3(i) + k1_2/2);k3_2 = h * \text{fewal}(f2, Y3(i) + k2_2/2);k4 2 = h*feval(f2,Y3(i)+k3_2);
YZ(i+1) = Y2(i)+(1/6)*(k1-2+2*k2-2+2*k3-2+k4-2);k1_3 = h*feval(f3,Y2(i),Y3(i),Y1(i));
 k2_3 = h*feval(f3,Y2(i)+k1_1/2,Y3(i)+k1_2/2,Y1(i)+k1_3/2);
 k3_3 = h*feval(f3,Y2(i)+k2_1/2,Y3(i)+k2_2/2,Y1(i)+k2_3/2);
k4_3 = h*fewal(f3,Y2(i)+k3_1,Y3(i)+k3_2,Y1(i)+k3_3);Y3(i+1) = Y3(i)+(1/6)*(k1_3+2*k2_3+2*k3_3+k4_3);end
% Plot results
plot(eta,Y1,eta,Y2,eta,Y3)
title("Plot of \eta versus Y1, Y2 and Y3")
grid on
xlabel('\eta')
ylabel('Y1,Y2,Y3')
legend('Y1','Y2','Y3')
plot(eta,Y1,'color', 'b')
title("Plot of \eta versus Y1")
grid on
xlabel('\eta')
ylabel('Y1')
plot(eta,Y2,'color', 'r')
title("Plot of \eta versus Y2")
grid on
xlabel('\eta')
ylabel('Y2')
plot(eta,Y3,'color', 'y')
title("Plot of \eta versus Y3")
grid on
xlabel('\eta')
ylabel('Y3')
```
### **5. Results and Discussions**

Using the numerical solution developed, we present a tabulation of 100 values of the results for F and its derivatives as a function of η.

$\eta$	F	F'	F''	$\eta$	F	F'	${\bf F}^{\prime\prime}$	$\eta$	$\mathbf{F}$	${\bf F}^{\prime}$	F''
$\boldsymbol{0}$	$\boldsymbol{0}$	$\boldsymbol{0}$	1.232	1.63	1.01	0.937	0.139	3.26	2.617	0.999	0.002
0.05	0.001	0.058	1.184	1.68	1.055	0.943	0.126	3.31	2.665	0.999	0.002
0.1	0.006	0.114	1.136	1.73	$1.1\,$	0.949	0.115	3.36	2.712	$\mathbf{1}$	0.002
0.14	0.012	0.167	1.089	1.78	1.146	0.954	0.105	3.41	2.76	$\mathbf{1}$	0.002
0.19	0.021	0.218	1.042	1.82	1.192	0.959	0.095	3.46	2.808	$\mathbf{1}$	0.001
0.24	0.033	0.267	0.995	1.87	1.238	0.963	0.086	3.5	2.856	$\mathbf{1}$	0.001
0.29	0.047	0.314	0.949	1.92	1.284	0.967	0.078	3.55	2.904	$\mathbf{1}$	0.001
0.34	0.063	0.358	0.904	1.97	1.331	0.971	0.07	3.6	2.953	$\mathbf{1}$	0.001
0.38	0.081	0.401	0.86	2.02	1.378	0.974	0.064	3.65	3.001	$\mathbf{1}$	0.001
0.43	0.102	0.441	0.817	2.06	1.424	0.977	0.057	3.7	3.049	$\mathbf{1}$	0.001
0.48	0.124	0.479	0.775	2.11	1.471	0.98	0.051	3.74	3.097	$\mathbf{1}$	0.001
0.53	0.148	0.516	0.734	2.16	1.518	0.982	0.046	3.79	3.145	$\mathbf{1}$	0.001
0.58	0.173	0.55	0.694	2.21	1.566	0.984	0.041	3.84	3.193	$\mathbf{1}$	0.001
0.62	0.2	0.582	0.656	2.26	1.613	0.986	0.037	3.89	3.241	$1\,$	$\boldsymbol{0}$
0.67	0.229	0.613	0.618	2.3	1.66	0.988	0.033	3.94	3.289	$1\,$	$\boldsymbol{0}$
0.72	0.259	0.642	0.582	2.35	1.708	0.989	0.029	3.98	3.337	$1\,$	$\boldsymbol{0}$
0.77	0.291	0.669	0.547	2.4	1.755	0.99	0.026	4.03	3.385	$\mathbf{1}$	$\boldsymbol{0}$
0.82	0.323	0.694	0.514	2.45	1.803	0.992	0.023	4.08	3.433	$\mathbf{1}$	$\boldsymbol{0}$
0.86	0.357	0.718	0.482	2.5	1.851	0.993	0.021	4.13	3.481	$\mathbf{1}$	$\boldsymbol{0}$
0.91	0.392	0.74	0.451	2.54	1.898	0.994	0.018	4.18	3.529	$\mathbf{1}$	$\boldsymbol{0}$
0.96	0.428	0.761	0.421	2.59	1.946	0.994	0.016	4.22	3.577	$\mathbf{1}$	$\boldsymbol{0}$
$1.01\,$	0.465	0.781	0.393	2.64	1.994	0.995	0.014	4.27	3.625	$\mathbf{1}$	$\boldsymbol{0}$
1.06	0.503	0.799	0.366	2.69	2.041	0.996	0.012	4.32	3.673	$\mathbf{1}$	$\boldsymbol{0}$
1.1	$\vert 0.542 \vert 0.816 \vert 0.341 \vert$					$2.74$   2.089   0.996	0.011	4.37	3.721	$1\,$	$\boldsymbol{0}$
1.15	0.582	0.832	0.316	2.78	2.137	0.997	0.01	4.42	3.769	$\mathbf{1}$	$\bf{0}$
1.2	0.622	0.847	0.294	2.83	2.185	0.997	0.008	4.46	3.817	$\mathbf{1}$	$\bf{0}$
1.25	0.663	0.86	0.272	2.88	2.233	0.998	0.007	4.51	3.865	$\mathbf{1}$	$\bf{0}$
1.3	0.705	0.873	0.251	2.93	2.281	0.998	0.006	4.56	3.913	$\mathbf{1}$	$\mathbf{0}$
1.34	0.747	0.884	0.232	2.98	2.329	0.998	0.006	4.61	3.961	$\mathbf{1}$	$\boldsymbol{0}$
1.39	0.789	0.895	0.214	3.02	2.377	0.999	0.005	4.66	4.009	$\mathbf{1}$	$\bf{0}$
1.44	0.833	0.905	0.197	3.07	2.425	0.999	0.004	4.7	4.057	$\mathbf{1}$	$\boldsymbol{0}$
1.49	0.876	0.914	0.181	3.12	2.473	0.999	0.004	4.75	4.105	$\mathbf{1}$	$\bf{0}$
1.54	0.92	0.922	0.166	3.17	2.521	0.999	0.003	4.8	4.153	$\mathbf{1}$	$\pmb{0}$
1.58	0.965	0.93	0.152	3.22	2.569	0.999	0.003				

**Table 1** Table of Results for non-dimensional Stream Function

Plots of the results for F and its derivatives as functions of η are also provided below.



**Figure 3** Plot of Stream Function together with its First and Second Derivatives



**Figure 4** Plot of Stream Function only



**Figure 5** Plot of first derivative of Stream Function only



**Figure 6** Plot of second derivative of Stream Function only

From the foregoing analysis, we can make the following inferences

- Near the wall, F increases at a very slow rate with η. This rate increases parabolically until it becomes linear at larger values of η.
- The first derivative of F initially increases linearly with η at lower values of η. The rate then decreases parabolically until F' eventually approaches a constant value of 1 as η increases.
- The second derivative of F becomes zero for large values of η.
- For plane stagnation flow, the similarity variable, η is defined as

$$
\eta = y \sqrt{\frac{k}{\nu}}
$$

- This shows that the similarity variable does not depend on the streamwise direction
- Also, the velocity components are defined as

$$
u = kxF'
$$

$$
v = -\sqrt{vk}F
$$

- Where ν is the kinematic viscosity and k is an arbitrary constant representing strain rate
- It is obvious from the above definition that the v-component of velocity depends only on the function F, and thus, increases with η at a slower (parabolic) rate for small values of η i.e., near the wall. This rate increases slightly and becomes linear for larger values of η.
- The u-component of velocity depends on x and F'. This means that for large values of η, u will depend only on the streamwise direction, x since F' approaches unity.

### **6. Conclusion**

In this study, we have successfully developed a numerical solution for the plane stagnation point flow using the fourth order Runge-Kutta approximation. The solution required numerical integration of the coupled first order ODEs with prescribed initial conditions. Our findings demonstrate that the proposed numerical approach effectively captures the key characteristics of the stagnation point flow, including the velocity distributions.

Overall, the numerical solution presented in this study offers a valuable tool for understanding and predicting the complex behavior of plane stagnation point flows. Future work can extend this approach to more complex geometry and boundary conditions, further enhancing its applicability in engineering and scientific research.

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